

# Turbulenzmodelle in der Strömungsmechanik

## Turbulent flows and their modelling

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## Summary of last lecture

### Lecture 6 – Wall-bounded shear flows

- ▶ What is the general structure of wall-bounded flows?
  - ▶ inner layer/outer layer: linear/log-law, defect law
- ▶ How does the presence of a solid boundary affect the turbulent motion?
  - ▶ stronger anisotropy than free shear flows
  - ▶ wall has selective effect on velocity components
- ▶ What is the effect of wall roughness?
  - ▶ shift of the log-law compared to smooth walls

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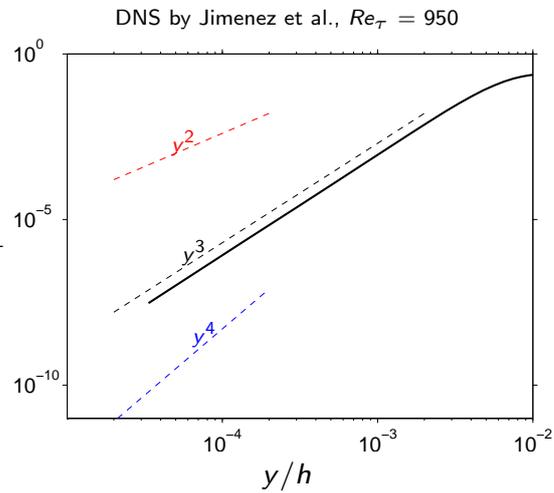
## Solution to last week's problem

Determine the variation with wall-distance of the production  $\mathcal{P}$  in fully-developed plane channel flow, valid for very small values of  $y$ .

Result:

$$\mathcal{P}(y) = \mathcal{O}(y^3) \quad \frac{\mathcal{P}}{u_\tau^3 / \delta_\nu}$$

for  $y/h \ll 1$



## LECTURE 7

### DNS as numerical experiments

## Questions to be answered in the present lecture

What are the possibilities & limitations of numerical simulations of the full Navier-Stokes equations?

- Part I
- ▶ what is DNS?
  - ▶ why perform DNS?
  - ▶ what is the history of DNS?
  - ▶ what are the computational requirements?
  - ▶ how to treat the boundary conditions?
- Part II
- ▶ DNS results for coherent structure dynamics in wall flows

## Definition of “direct numerical simulation”

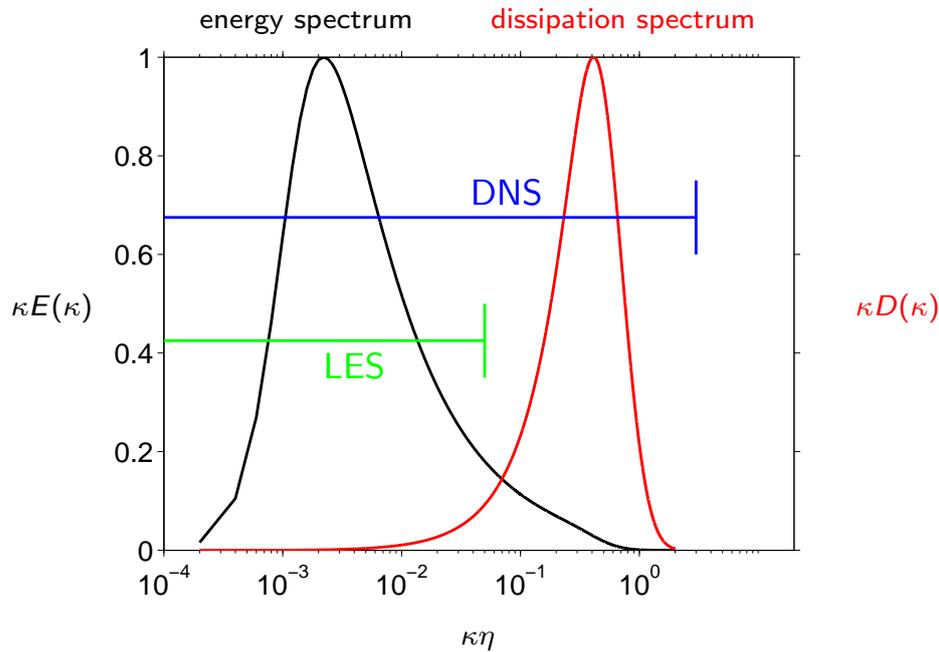
Solve the Navier-Stokes equations for turbulent flow, resolving all relevant temporal and spatial scales.

- ▶ for incompressible fluid solve:

$$\begin{aligned}\partial_t \mathbf{u} + (\mathbf{u} \cdot \nabla) \mathbf{u} + \frac{1}{\rho} \nabla p &= \nu \nabla^2 \mathbf{u} \\ \nabla \cdot \mathbf{u} &= 0\end{aligned}$$

with suitable initial & boundary conditions.

## Spectral view: DNS versus LES

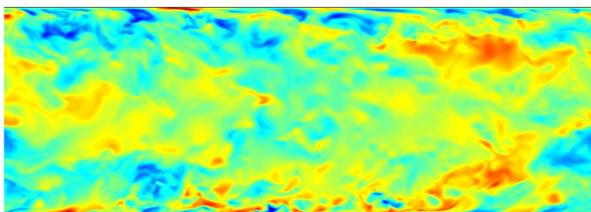


- ▶ DNS resolves spatial scales down to Kolmogorov scale  $\eta$

## Physical space view: DNS versus RANS

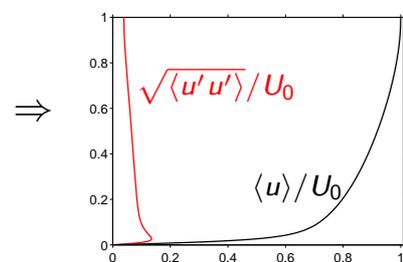
Example: channel flow

instantaneous DNS data ( $u'$ )



→ flow direction

DNS statistics



- ▶ DNS needs to be integrated in time to obtain statistics
- ▶  $\langle u_i \rangle$ ,  $\langle u'_i u'_j \rangle$  are variables in RANS computation

## Objectives of DNS studies

(Today) DNS is a research method, not an engineering tool.

- ▶ computational effort:
  - today not feasible to perform DNS for practical application
- ▶ main purpose of DNS:
  - development of turbulence theory
  - ⇒ improvement of simplified models

## 1. DNS as “precise experiment” or “perfect measurement”

If we can simulate the flow with high-fidelity:

- ▶ full 3D, time-dependent flow field is available
  - ▶ virtually any desired quantity can be computed (e.g. pressure fluctuations, pressure-deformation tensor)
  - ▶ there are no limitations by measurement sensitivity (e.g. size of probes near a wall)
  - ↔ analysis only limited by mind of researcher (it is important to ask the right questions)
- ⇒ DNS complements existing laboratory experiments

## 2. DNS as “virtual experiment”

When experiments are too costly/impossible to realize:

- ▶ numerical simulations provide great flexibility
- ▶ idealizations can be realized with ease:
  - ▶ e.g. homogeneous-isotropic flow conditions
  - ▶ periodicity
  - ▶ absence of gravitational force
  - ▶ ...

⇒ DNS replaces laboratory experiments

## 3. DNS as “non-natural experiment”

When non-physical configurations need to be simulated:

- ▶ we have the possibility to modify the equations
- ▶ we can apply arbitrary constraints
- ▶ examples from the past are:
  - ▶ filtering (damping) turbulence in some part of the domain
  - ▶ suppress individual terms in the equations
  - ▶ applying artificial boundary conditions
  - ▶ ...

⇒ DNS directly serves turbulence theory

## Historical development of DNS

1972 first ever DNS of hom.-iso. turbulence by Orszag & Patterson

1981 homogeneous shear flow by Rogallo

1987 plane channel flow by Kim, Moin & Moser

1986-88 flat-plate boundary layer by Spalart

1990-95 homogeneous compressible flow (Erlebacher/Blaisdell/Sarkar)

1997 particle transport in channel flow (Pan & Banerjee)

2005 deformable bubbles in channel flow (Lu et al.)

currently: wide range of configurations ...

- ▶ # of publications in Phys. Fluids: 1990 – 14, 2008 – 76

## Numerical requirements for DNS

### Homogeneous turbulence

- ▶ uniform grid with  $N \times N \times N$  points:

$$\Delta x = \Delta y = \Delta z = \frac{\mathcal{L}}{N}$$

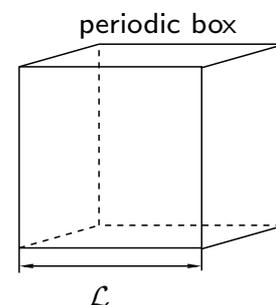
- ▶ assume a periodic field

→ use Fourier series with wavenumbers:

$$\kappa_i^{(\alpha)} = \frac{2\pi i}{\mathcal{L}}, \text{ where: } -N/2 \leq i \leq N/2$$

⇒ largest wavenumber:  $\kappa_{max} = \frac{\pi N}{\mathcal{L}}$

- ▶ operation count per time step: using fast Fourier transform  $\mathcal{O}(N^3 \log N)$



Fourier modes:  $\exp(i\kappa x)$

$$\kappa = (\kappa^{(1)}, \kappa^{(2)}, \kappa^{(3)})$$

## Homogeneous turbulence – spatial resolution

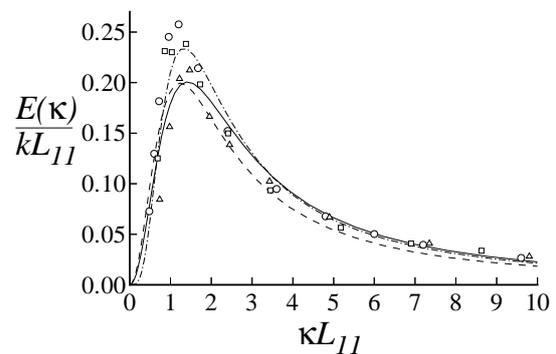
### Large scale resolution

- ▶ largest flow scales need to be much smaller than box size
- ↪ otherwise: artifacts of periodicity!
- ▶ rule of thumb: (box)  $\mathcal{L} \geq 8L_{11}$  (integral scale)
- ▶ recall: largest non-zero wavenumber in DNS is  $\kappa_0 = \frac{2\pi}{\mathcal{L}}$
- ⇒  $\kappa_0 L_{11} = \frac{\pi}{4}$
- found to be adequate by comparison with experiments

## Homogeneous turbulence – large scale resolution (2)

### Energy-containing range

- ▶ smallest wavenumber:  
 setting  $\kappa_0 L_{11} = \frac{\pi}{4}$
- ⇒  $\approx 95\%$  of energy resolved



grid turbulence, Comte-Bellot & Corrsin 1971

○  $Re_\lambda = 60 \dots 70$

## Homogeneous turbulence – small scale resolution

### Small scale resolution

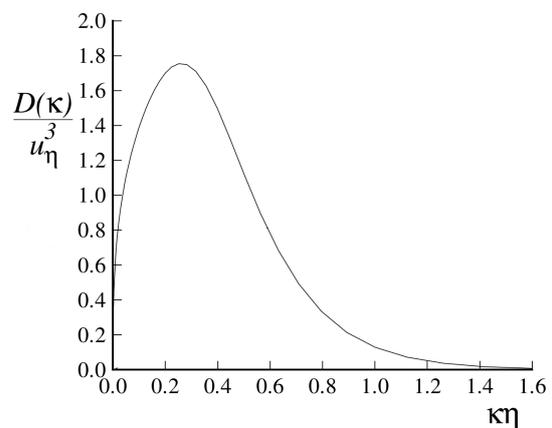
- ▶ need to resolve the dissipation range
- ↪ otherwise: there is no sink for kinetic energy → “pile-up”
- ▶ rule of thumb:  $\kappa_{max}\eta \geq 1.5$  or  $\Delta x \leq \frac{\pi\eta}{1.5}$

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## Homogeneous turbulence – small scale resolution (2)

### Dissipation range

- ▶ representing up to:  
 $\kappa_{max}\eta = 1.5$
- ⇒ most dissipation resolved



Pope's model spectrum,  $Re_\lambda = 600$

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## Homogeneous turbulence – number of grid points

### Combined small/large scale requirements

$$\blacktriangleright N = \frac{\mathcal{L}}{\Delta x} = \frac{12L_{11}}{\pi\eta}$$

- ▶ how does the scale ratio  $L_{11}/\eta$  evolve with  $Re$ ?
- ▶ from the model spectrum:  $L_{11}/L \approx 0.43$  for large  $Re$   
(recall  $L \equiv k^{3/2}/\varepsilon$  from lecture 6)
- ▶ defining  $Re_L \equiv \frac{k^{1/2}L}{\nu}$  we obtain:  $\frac{L}{\eta} = Re_L^{3/4}$

$$\Rightarrow \text{finally: } \boxed{N \approx 1.6 Re_L^{3/4}} \text{ i.e. } \boxed{N^3 \approx 4.4 Re_L^{9/4}}$$

↪ steep rise with Reynolds!

## Homogeneous turbulence – temporal resolution

### Resolving the small-scale motion

- ▶ typically need: (time step)  $\Delta t = 0.1\tau_\eta$  (Kolmogorov scale)

### Sampling sufficient large-scale events

- ▶ each simulation needs to be run for a time  $T$  given by:  
$$T \approx 4 \frac{k}{\varepsilon} \quad (k/\varepsilon \text{ is characteristic of large scales})$$

⇒ obtain for the number of time steps  $M$ :

$$\blacktriangleright \boxed{M = \frac{T}{\Delta t} = \frac{4}{0.1} Re_L^{1/2}}$$

## Homogeneous turbulence – total operation count

Total number of operations per DNS, using spectral method:

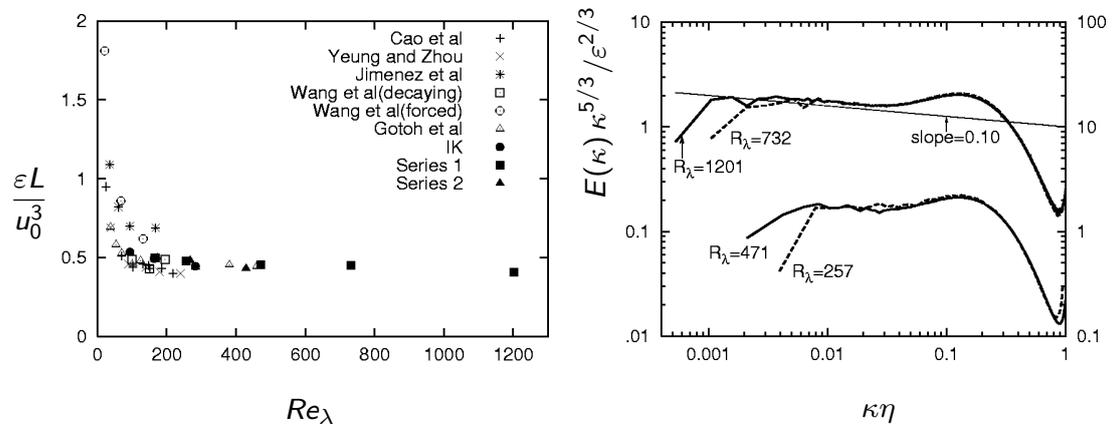
$$\blacktriangleright N_{tot} = N_{op} \cdot M \sim N^3 \log(N) \cdot M \sim Re_L^{11/4} \log(Re_L)$$

Simulation parameters for “landmark” studies:

$N$	$Re_L$	computer speed	# processors	
32	180	10 Mflop/s	1	Orszag & Patterson 1972
512	4335	46 Gflop/s	512	Jimenez et al. 1993
4096	216000	16 Tflop/s	4096	Kaneda et al. 2003

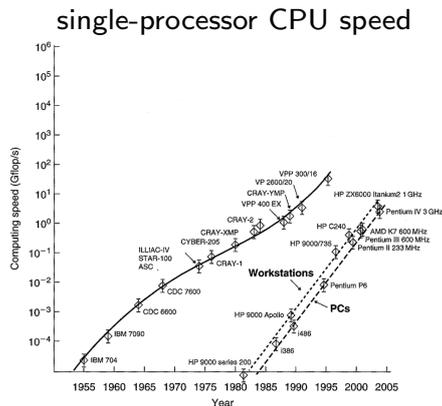
## Result of high-Reynolds DNS of hom.-iso. turbulence

Kolmogorov scaling of data by Kaneda et al. (2003)

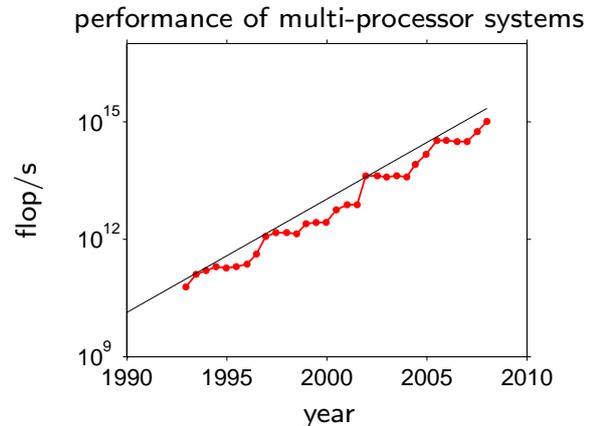


$\blacktriangleright$  scaling largely confirmed

## Evolution of computer speed



(from Hirsch 2007)



(data from top500.org)

- ▶ large CPU speed increase
- ▶ limitation: power & heat

- ▶ massively-parallel machines maintain exp-growth

⇒ peak performance doubles every 18 months

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## Boundary conditions for DNS

No particular problems posed by the following boundaries:

- ▶ solid walls, homogeneous directions, far-field

The problem of inflow-outflow boundaries:

we need to prescribe turbulence!

1. Taylor's hypothesis → temporal instead of spatial variation
2. rescaled outflow used as inflow (Spalart) → works for BL
3. impose artificial turbulence at inflow (Le & Moin) → long evolution length
4. periodic companion simulation (Na & Moin) → generates inflow

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## Wall turbulence – numerical requirements

Number of grid points, using spectral method:

$$\blacktriangleright N^3 \approx 0.01 Re_\tau^3 \left(\frac{L_x}{h}\right) \left(\frac{L_z}{h}\right)$$

Total number of operations per DNS, using spectral method:

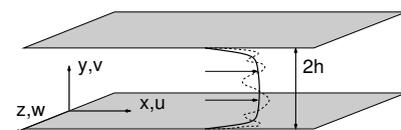
$$\blacktriangleright N_{tot} \sim Re_\tau^4 \left(\frac{L_x}{h}\right)^2 \left(\frac{L_z}{h}\right)$$

Simulation parameters for “landmark” studies:

$N^3$	$Re_\tau$	$L_x/h$	$L_z/h$	
$4 \cdot 10^6$	180	$4\pi$	$2\pi$	Kim, Moin & Moser 1987
$3.8 \cdot 10^7$	590	$2\pi$	$\pi$	Moser, Kim & Mansour 1999
$1.8 \cdot 10^{10}$	2000	$8\pi$	$3\pi$	Hoyas & Jimenez 2006

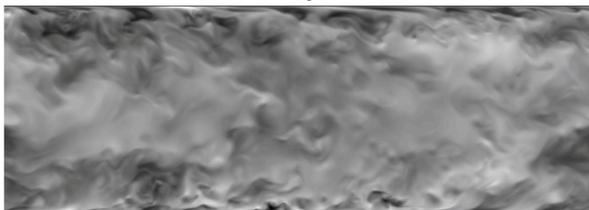
## Wall turbulence – visualization

Channel flow at  $Re_\tau = 590$



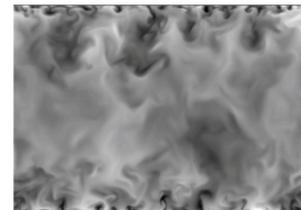
- ▶ visualizing streamwise velocity fluctuations  $u'$

x-y slice



→ flow direction

z-y slice

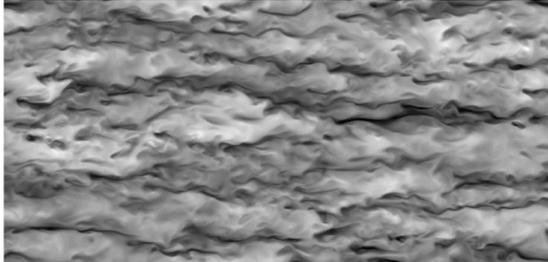


⊗ flow direction

## Wall turbulence – visualization (2)

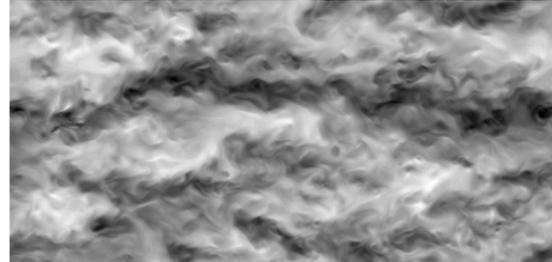
Channel flow at  $Re_\tau = 590$ , wall-parallel planes,  $u'$

x-z slice, wall-distance  $y^+ = 45$



→ flow direction

x-z slice, wall-distance  $y^+ = 170$



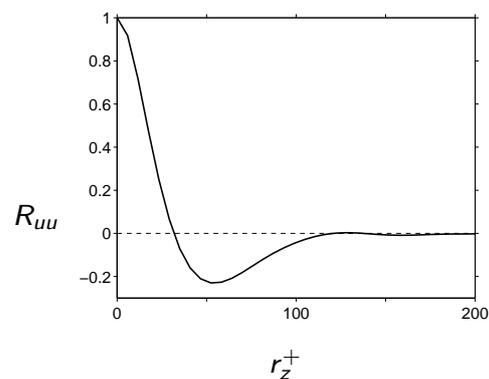
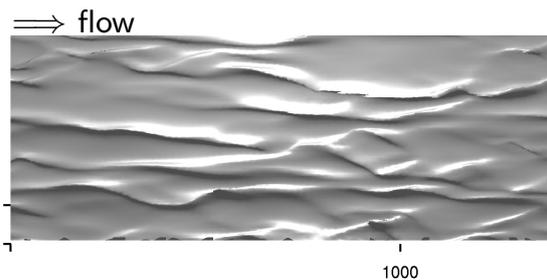
→ flow direction

- ▶ typical structures: streamwise velocity “streaks”
- found in all boundary-layer type flows

## Facts about velocity streaks in the buffer layer

Statistically speaking:

- ▶ lateral spacing of streaks:  
 $\Delta l_z^+ \approx 100$
- ▶ how do we know?
- ⇒ two-point correlations:  
 minimum of  $R_{uu}$  at  
 half of the streak spacing

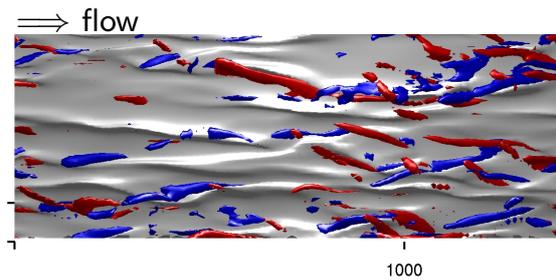
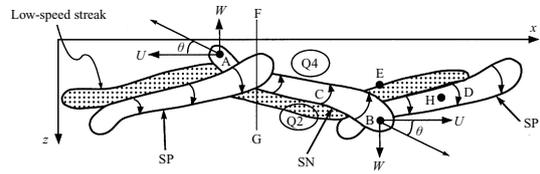


(Moser et al. 1999)

# Streamwise vortices

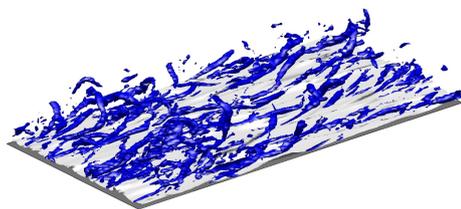
- Streamwise vortices ( $\omega'_x$ )
- $l_x^+ \approx 200$
- ▶ associated with streaks

(from Jeong et al. 1997)

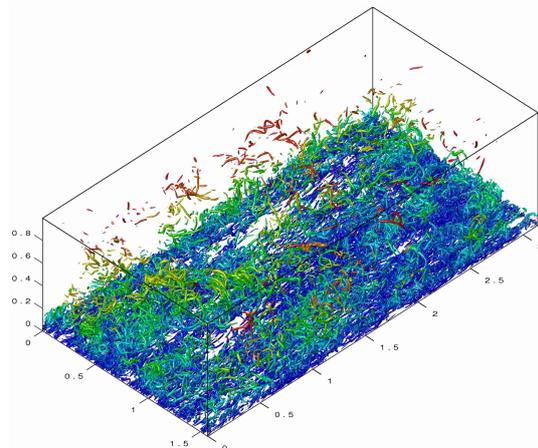


# Complex vortex tangles at different Reynolds numbers

$Re_\tau = 180$



$Re_\tau = 1900$

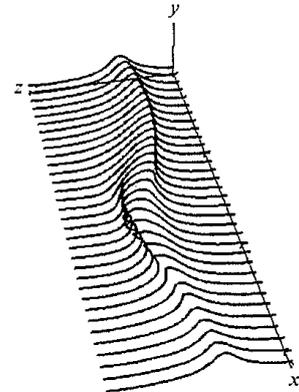
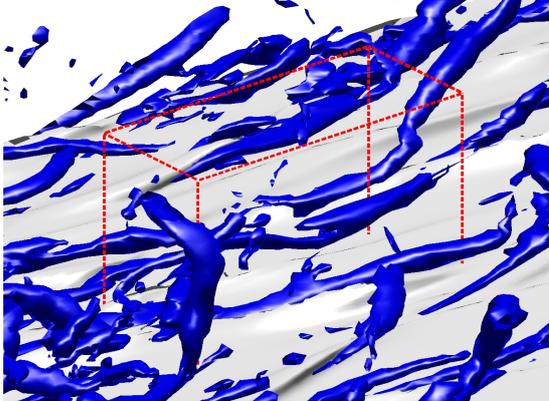


(from del Alamo et al. 2006)

(movie)

## Sometimes less is more: reducing the complexity

The “minimal flow unit” of Jimenez & Moin



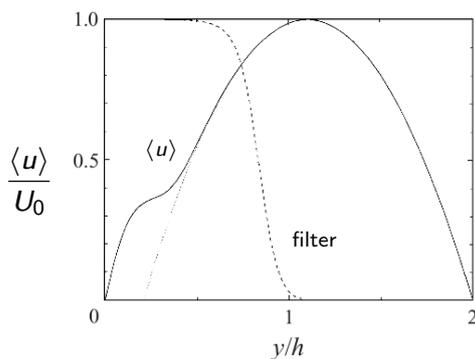
(from Jimenez & Moin 1991)

- ▶ reducing the box size to a minimum without relaminarizing
- ▶  $\min L_x^+ \approx 350$ ,  $\min L_z^+ \approx 100$
- ⇒ cheap “laboratory” with principal buffer layer features

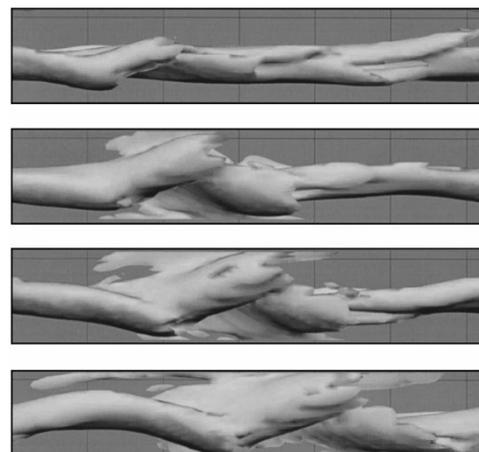
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## Sometimes wrong is right: manipulating the equations

The “autonomous wall” of Jimenez & Pinelli (1999)



- ▶ suppress  $u'$  for  $y^+ \geq 60$
- ⇒ turbulence survives!
- ▶ near-wall region: statistics approximately unchanged

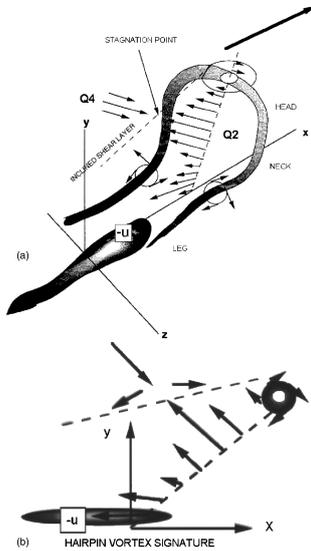


- ▶ time sequence of streak break-up (movie)

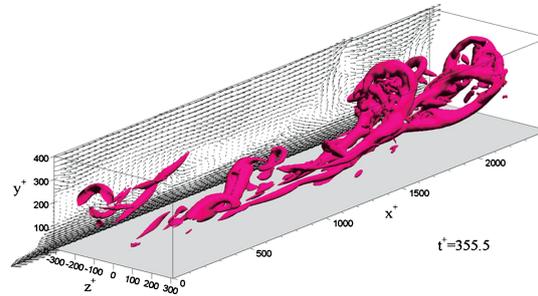
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## What happens outside the buffer layer?

### Hairpin vortices growing into vortex packets



(sketch from Adrian 2007)



(DNS by Adrian 2007)

- ▶ structures in outer region still under investigation!

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## How can we apply knowledge about coherent structures?

### Control of turbulent flow

- ▶ “opposition control” (Choi, Moin & Kim 1994)
- ▶ imposing  $v_{wall}(x, z) = -v'(x, y^+ = 10, z)$
- up to 25% drag reduction
- ↔ but: this method is not practical
- ▶ other feasible techniques exist, where sensing is performed at the wall

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## Reduced order models of the wall region

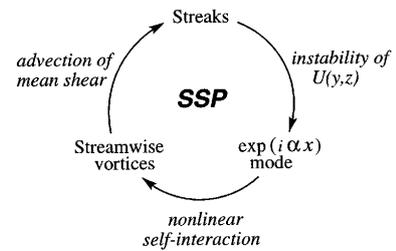
### Waleffe's self-sustained process

- ▶ generic mechanism
- ▶ streamwise vortices generate streaks by advection
- ▶ streaks are unstable to sinusoidal perturbations
- ▶ perturbations generate new vortices by self-interaction

→ 4-equ. model for artificial flow

↔ but: not feasible in practice

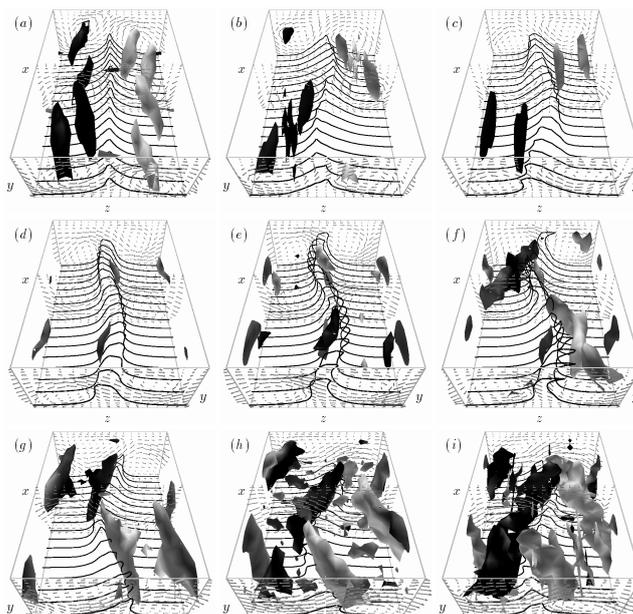
⇒ similar models could be used with LES in future ...



(from Waleffe 1997)

## Periodic solutions: "building blocks" for future models?

Exact periodic solutions are currently pursued in various flows



(movie)

(one period of a Couette flow solution, from Kawahara et al. 2006)

## Summary

### Main issues of the present lecture

- ▶ DNS is useful as a research tool
  - ▶ precise experiment/perfect measurement
  - ▶ virtual experiment
  - ▶ non-natural experiment
- ▶ estimates of operation count rise sharply with Reynolds
- ▶ suitable inflow boundary conditions are difficult to generate
- ▶ streaks & streamwise vortices are fundamental ingredients of turbulence regeneration cycle

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## Outlook on next lecture: Introduction to RANS modelling

How can the Reynolds-averaged equations be closed?

What are the different types of models commonly used?

Do simple eddy viscosity models allow for acceptable predictions?

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## Further reading

- ▶ S. Pope, *Turbulent flows*, 2000  
→ chapter 9 & 7.4
- ▶ P. Moin and K. Mahesh, *DNS: A tool in turbulence research*,  
Annu. Rev. Fluid Mech., 1998, vol 30, pp. 39.
- ▶ this is a very active area; more information can be found in  
the current research literature (Journal of Fluid Mechanics,  
Physics of Fluids, Journal of Computational Physics)